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## In the claims:

Please amend the claims as shown below:

- 5 1. (Currently amended) A method for dewatering and washing a lime mud (106) before dewatered lime mud is transported to a lime mud kiln, comprising: (200) characterised in that the dewatering of the lime mud takes place in a pressurised pressurized filter (102),
- that the pressurised connecting the pressurized filter (102) is connected to a closed gas circulation system (101), that connecting a filtrate tank (108) is connected to a the filtrate side of the pressurized filter and where a fluid level of filtrate (109) is established from the pressurised pressurized filter (102),
- that the pressurised pressurizing the pressurized filter,
  - a compressor (111) <u>drawing</u> on the <u>a</u> suction side <u>thereof</u> <u>a</u> draws gas phase from the filtrate tank, (108) and <u>a</u>
- 20 pressurized side of the compressor pressurizing, via the cas circulation system, a lime mud side of pressurises the pressurized filter.
  - (102) on the pressurised side of the compressor, on the lime mud side of the filter, that a certain
- 25 <u>venting a</u> pre-determined amount of <u>the</u> gas phase <del>is vented</del> from the gas circulation system (101), and that <u>added</u> an equivalent pre-determined amount of fresh air is added to the <u>a</u> recycled gas phase <u>to with the aim of the transfer.</u>
- maintaining the <u>a</u> partial pressure of oxygen gas above a pre-
  - 2. (Currently amended) The method according to claim 1,

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characterised in that the wherein a temperature in the pressurized pressurised filter (102), including a the temperature of the recycled gas phase, is maintained above 75°C, preferably 75°95°C.

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- 3. (Currently amended) The method according to sither claim 1 or 2, characterised in that the claim 1 wherein an amount of residual white liquor in the lime mud (106) does not exceed 10%, preferably under 5%, of the white liquor that is formed in the a previous causticization step.
- 4. (Currently amended) The method according to any one of claims 1-3, characterised in that claim 1 wherein the lime mud that has been filtered out from the lime mud is dry-fed out from the a disc filter for onwards transportation to the lime mud kiln (300).
- 5. (Currently amended) The method according to any one of claims 1-4, characterised in that claim 1 wherein de-airing of the recycled gas phase is carried out on the pressurized pressurized side (p) of the compressor via a de-airing device (113a), and in that and an addition of fresh air is carried out by an air-supply device (112a) connected to the suction side (s) of the compressor.

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6. (Currently amended) The method according to any one of claims 1-4. characterised in that claim 1 wherein de-airing of recycled gas phase is carried out on the suction side (8) of the compressor at a first distance from the an inlet to the compressor via a de-airing device (113a), and in that and an addition of fresh air is carried out through an air-supply device (112a) on the suction side (8) of the

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compressor at a second distance from the an inlet to the compressor, where the first distance is greater than the second distance.

- 7. (Currently amended) The method according to any one of the preceding claims, characterised in that the claim 1 wherein an amount of recirculated gas phase that is exchanged lies within the an interval 5-20%, preferably less than 10%.
- 8. (Currently amended) The method according to any one of the proceeding claims, characterised in that the claim 1 wherein an amount of recirculated gas phase that is exchanged is regulated such that 15 the amount depends on a detected process parameter.
- 9. (Currently amended) The method according to claim 8, characterised in that wherein the detected process parameter is the partial pressure of oxygen gas in the pressurized filter.
- 10. (Currently amended) The method according to claim 8, characterised in that wherein the detected process parameter is the a flow rate of flow of lime mud or dewatered lime mud, or parameters that are representative of these flow rates of flow.
  - 11. (Currently amended) The method according to any one of the preceding claims, characterised in that claim 1 wherein the pressurized pressurised filter is of the a disc filter type.

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12. (Currently amended) An arrangement for washing and dewatering a lime mud before dewatered lime mud is transported to a lime mud kiln, comprising: (200) characterised in that the dewatering of the lime mud takes place in a pressurised pressurized filter (102),

that arranging a recirculation line 110 is arranged for a gas phase from the a filtrate side to the of a mud side, that connecting the pressurised pressurized filter (102) is connected to a gas circulation system (101) that is

10 essentially closed,

that <u>connecting</u> a filtrate tank (100) is connected to the
a filtrate side of the <u>pressurized</u> filter and where a fluid
level of a filtrate (100) is established from the <u>pressurized</u>
pressurized filter, (102),

15 that pressurizing the pressurised pressurized filter, (102) is pressurised in that

a compressor (111) drawing on its a suction side thereof a draws gas phase from the filtrate tank (108) and pressurises a pressurized side of the compressor pressurizing, via the gas circulation system a lime mud side of the pressurized filter, (102) on the pressurised side of the compressor, on the lime

mud side of the filter,

that venting a certain pre-determined amount of gas phase is vented from the gas circulation system (101), through  $\underline{a}$  de-airing devices, (113a) and

that adding an equivalent pre-determined amount of fresh air is added through an air-supply devices (112a) to the a recycled gas phase with to maintain a the aim of maintaining the partial pressure of oxygen gas above a pre-determined minimum level.

minimum level.

13. (Currently amended) The arrangement according to claim 12, characterised in that wherein the de-airing device (113a) is

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arranged at a position on the <u>pressurized pressurised</u> side (p) of the compressor, and in that the air-supply device (112a) is arranged at a position on the suction side (s) of

the compressor.

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14. (Currently amended) The arrangement according to claim 12, characterised in that wherein the de-airing device (113a) is arranged at a position on the suction side (s) of the compressor at a first distance from the compressor (111), and in that the air-supply device (112a) is arranged at a position on the suction side (s) of the compressor at a second distance from the compressor (111), where the first distance is greater than the second distance.

- 15 (Currently amended) The arrangement according to any one of claims 12-14, characterised in that claim 12 wherein a control unit (140) controls the regulator valves (112), (150) for at least one of de-airing and addition of air.
  - 16. (Currently amended) The arrangement according to claim 15, wherein characterised in that the control unit 140 receives input signals from sensors 150.
- 25 17. (Currently amended) The arrangement according to <u>claim 12</u> wherein the pressurized any one of claims 12-16, characterised in that the pressurised filter (102) is of a the disc filter type.